

CLAIMS

1. A process for producing a siliceous layer capable of biomass immobilization and selectively cutting off macromolecules having a molecular weight higher than a selected threshold, comprising the steps of:
- 5 a) supplying a gas flow of a gas carrier saturated by a mixture of silicon alkoxides selected from the group comprising (1) $\text{Si}(\text{OR})_4$, (2) $\text{SiH}(\text{OR})_3$, (3) $\text{R}'\text{Si}(\text{OR})_3$ and (4) $\text{R}'\text{SiH}(\text{OR})_2$ wherein R and R', equal or different
- 10 each other, are alkyl and/or aryl groups, wherein said gas flow is prepared by bubbling the gas carrier into a liquid mixture of said alkoxides in the ratio of (1) 40-85/(2) 0-60/(3) 0-60/(4) 0-60 (% v/v), at a temperature of from 20 to 180°C, preferably of from 20
- 15 to 100°C, and
- b) exposing a support comprising a biomass to the gas flow of step a),
- wherein said selected threshold of molecular weight is chosen in the range of between 10,000 Dalton and 150,000
- 20 Dalton and wherein the ratio between the (1), (2), (3) and (4) Si derivatives in step a) is chosen as a function of the molecular weight of the macromolecules to be cut off.
2. A process according to claim 1, wherein R is ethyl or
- 25 methyl and R' is methyl.

3. A process according to claim 1 or claim 2, wherein the ratio between the (1), (2), (3) and (4) Si derivatives in step a) is chosen in order to cut off macromolecules having a molecular weight higher than 10,000 Dalton.
- 5 4. A process according to claim 1 or claim 2, wherein the ratio between the (1), (2), (3) and (4) Si derivatives in step a) is chosen in order to cut off macromolecules having a molecular weight higher than 70,000 Dalton.
- 10 5. A process according to claim 1 or claim 2, wherein the ratio between the (1), (2), (3) and (4) Si derivatives in step a) is chosen in order to cut off macromolecules having a molecular weight higher than 90,000 Dalton.
- 15 6. A process according to claim 1 or claim 2, wherein the ratio between the (1), (2), (3) and (4) Si derivatives in step a) is chosen in order to cut off macromolecules having a molecular weight higher than 150,000 Dalton.
- 20 7. A process according to any one of claims 1, 2 and 6, wherein the content of $R'Si(OR)_3$ derivative in step a) is up to about 10% v/v and it is added in replacement of a same amount of $Si(OR)_4$.
8. A process according to claim 7, wherein the Si derivatives in step a) are $Si(OR)_4/R'SiH(OR)_2/R'Si(OR)_3$ in a ratio of 65-79% / 20-25% / 1-10% v/v.
- 25 9. A process according to any one of claims 1 to 6, wherein the content of $R'Si(OR)_3$ derivative in step a)

is between about 10% v/v and about 20% v/v and it is added in replacement of a same amount of Si(OR)_4 .

10. A process according to claim 9, wherein the Si derivatives in step a) are $\text{Si(OR)}_4/\text{R'SiH(OR)}_2/\text{R'Si(OR)}_3$ in a ratio of 53-70% / 15-25% / 10-22% v/v.
11. A process according to any one of claims 1, 2 and 5, wherein the content of R'Si(OR)_3 derivative is 0%.
12. A process according to any one of claims 1 to 11, wherein the total gas flow of step a) is of from 0.05 to 10 L/min for exposing times corresponding to from 1 to 100 mL of total gas per square centimeter of exposed surface.
13. A process according to any one of claims 1 to 12, wherein the support of step b) is a matrix which adheres to a scaffolding material.
14. A process according to any one of claims 1 to 13, wherein the support of step b) is a matrix in form of microsphere having preferably a diameter of from 0.05 to 1.0 mm.
15. A process according to claim 14, wherein the matrix in form of microsphere is without a scaffolding material.
16. A process according to any one of claims 1 to 12, wherein the support of step b) is a scaffolding material without a matrix and the biomass is directly supported on said scaffolding material.

17. A process according to any one of claims 1 to 16, wherein the siliceous layer has a thickness of from 0.01 to 10 μm , preferably from 0.05 to 0.3 μm .
18. A process according to any one of claims 1 to 17, wherein the siliceous layer has a critical shear thinning stress higher than 10 Pa, preferably a shear thinning stress of from 12 to 20 Pa.
19. A process according to any one of claims 1 to 18, wherein the said carrier gas is air.
- 10 20. A bioreactor comprising a biomass immobilized by a siliceous layer as obtainable by the process described in any one of claims 1 to 19.
21. A bioreactor according to claim 20, wherein the bioreactor is an artificial organ or tissue, or is a cell aggregate which may also be genetically modified.
- 15 22. An implantable bioreactor according to claim 20 or claim 21, wherein the support is a matrix in form of microspheres.
23. Use of the bioreactor according to claim 22 for preparing an injectable pharmaceutical composition for performing a function of biological type.
- 20 24. An injectable pharmaceutical composition comprising an effective amount of the bioreactor according to claim 22 suspended in a physiological solution.
- 25 25. An injectable pharmaceutical composition according to

claim 24, wherein the microspheres have a diameter of from 0.05 to 1.0 mm.

26. An injectable pharmaceutical composition according to claims 24 and claim 26, wherein the amount of
5 microspheres is of from 100 to 50,000 microspheres/ml of physiological solution.